

Nonlinear Model Predictive Control of an Adiabatic CSTR

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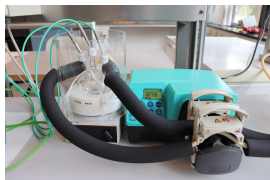
2019-01-14

About Eskild

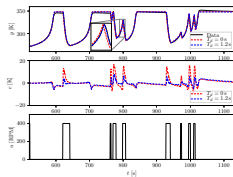
- ▶ Chemical engineer from the Technical University of Denmark 2017
- ▶ Research assistant at DTU Compute July to September 2017
- ▶ Employed at Novo Nordisk in Hillerød

I am not affiliated with any research institution. The presentation is the result of an effort in my spare time.

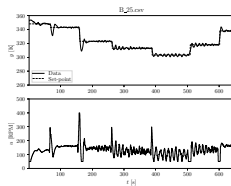
Key points and learnings



Novel system for experimental evaluation of NMPC.

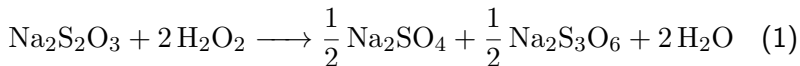
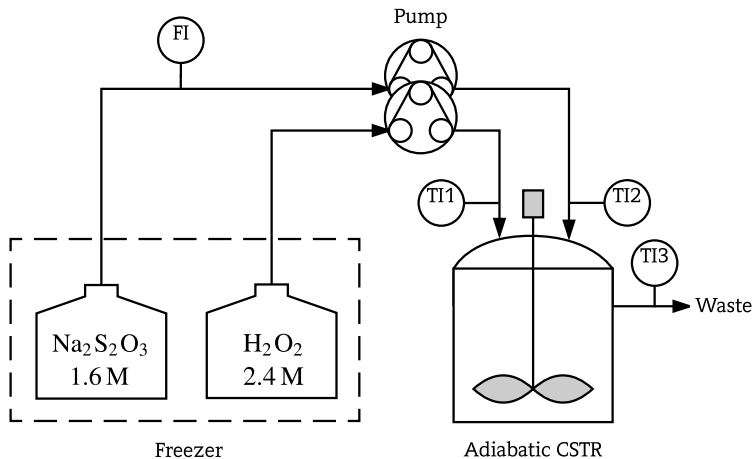


A non-linear model with input time delay.

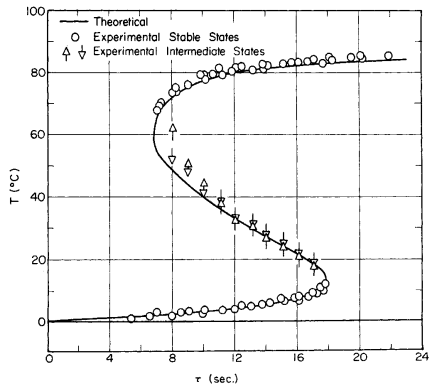
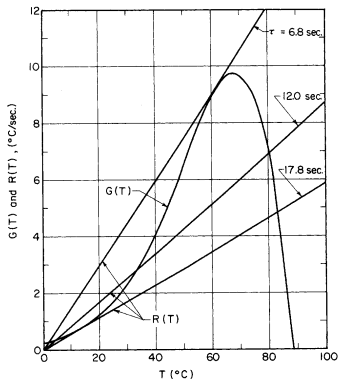


Unstable system stabilized with NMPC.

Topic for today



Topic for today



S. A. Vejtasa and R. A. Schmitz, *AIChE Journal*, 1970

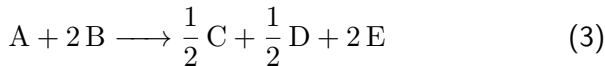
- ▶ Relatively easy to perform experiments
- ▶ The goal: To control the temperature to any set-point.

How to achieve the goal?

$$\begin{aligned} \min_{x, u} \quad & \frac{1}{2} \sum_{i=0}^{N-1} x_i^T Q_c x_i + u_i^T Q_u u_i dt + \frac{1}{2} x_N^T Q_f x_N \\ \text{s.t.} \quad & x_0 = \hat{x}_0 \\ & x_{i+1} = f(x_i, u_i), \quad i = 0, \dots, N-1 \\ & u_{\min} \leq u_i \leq u_{\max}, \quad i = 0, \dots, N-1 \\ & \Delta u_{\min} \leq u_{i+1} - u_i \leq \Delta u_{\max}, \quad i = 0, \dots, N-2 \end{aligned}$$

Model

Consider the reaction as



with 2nd order reaction rate

$$-r_A = c_A c_B \exp\left(A - \frac{B}{T}\right) \quad (4)$$

Then mass/energy balances for CSTR conditions are

$$\frac{dT}{dt} = \frac{q}{V}(T_{\text{in}} - T) + \frac{(-\Delta H_r)}{\rho c_p} c_A c_B \exp\left(A - \frac{B}{T}\right) \quad (5a)$$

$$\frac{dc_A}{dt} = \frac{q}{V}(c_{A,\text{in}} - c_A) - c_A c_B \exp\left(A - \frac{B}{T}\right) \quad (5b)$$

$$\frac{dc_B}{dt} = \frac{q}{V}(c_{B,\text{in}} - c_B) - 2 c_A c_B \exp\left(A - \frac{B}{T}\right). \quad (5c)$$

Model

Further assume constant T_{in} , $c_{A,\text{in}}$ and $c_{B,\text{in}}$ yielding:

$$\frac{dT}{dt} = \frac{q}{V} (T_{\text{in}} - T) + \theta R(T) \quad (6a)$$

with reaction rate and parameters

$$R(T) = 2 c_{B,\text{in}} \left(1 - \frac{T - T_{\text{in}}}{\theta}\right) \left(\phi - \frac{T - T_{\text{in}}}{2\theta}\right) \exp\left(A - \frac{B}{T}\right) \quad (6b)$$

$$\phi = \frac{c_{A,\text{in}}}{c_{B,\text{in}}} \quad (6c)$$

$$\theta = \frac{(-\Delta H_r) c_{B,\text{in}}}{2 \rho c_p} \quad (6d)$$

This model presents multiple advantages:

- ▶ The assumptions are plausible
- ▶ Just one temperature measurement is required
- ▶ The model is unidimensional

Model assumptions

The model rests on certain equipment specific assumptions:

- ▶ State is measurable instantaneously
- ▶ Reactor is adiabatic
- ▶ Good correlation between pump set-point and throughput

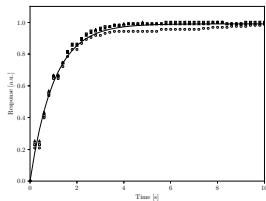


Figure: Thermocouple time constant approximately 1 s.

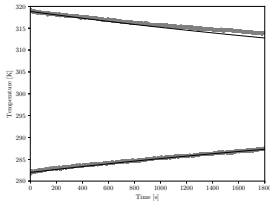


Figure: Reactor is approximately adiabatic.

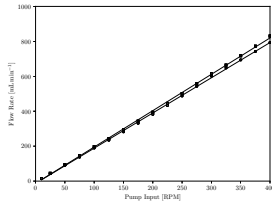


Figure: Pump response is linear and similar for both feeds.

Identification

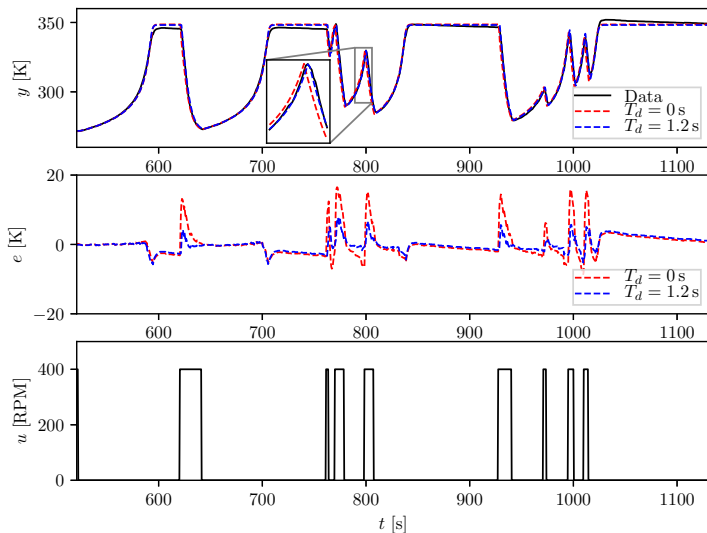
- ▶ Step response experiment
- ▶ Reasonable parameter estimates are available
- ▶ Accuracy of models for similar systems has been shown to be good
- ▶ Fit via least squares

Identification experiment is constructed based on a binary input signal subject to a desired output excitation profile.

Table: Nominal model parameters.

Parameter	Nominal value
V	105 mL
$c_{A, \text{in}}$	$\frac{1.6}{2} \text{ mol L}^{-1}$
$c_{B, \text{in}}$	$\frac{2.4}{2} \text{ mol L}^{-1}$
T_{in}	0.5°C
ρ	1 kg L ⁻¹
c_p	4186 J (kg K) ⁻¹
A	24.6 L (s mol) ⁻¹
B	8500 K
ΔH_R	-560 kJ mol ⁻¹

Identification experiment



The fit appears to be very good, especially when a time-delay is incorporated into the model.

Integration of ODE with constant input time delay

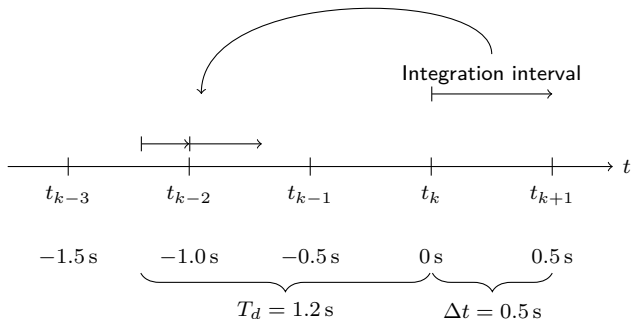
Parameters:

▶ $\Delta t = 0.5 \text{ s}$

▶ $T_d = 1.2 \text{ s}$

$n = 2$, $\frac{T_d}{\Delta t} = 2.4$ is non-integer.

1. Integrate over the interval 0.2 s using $q = u(t_{k-3})$
2. Integrate over the interval 0.3 s using $q = u(t_{k-2})$



Model for State Estimation (EKF)

Model and disturbance model

$$\frac{dT}{dt} = \frac{q}{V} (T_{\text{in}} - T) + \theta R(T) + x_d \quad (7a)$$

$$\frac{dx_d}{dt} = 0 \quad (7b)$$

Reaction rate and parameters

$$R(T) = 2 c_{B, \text{in}} \left(1 - \frac{T - T_{\text{in}}}{\theta} \right) \left(\phi - \frac{T - T_{\text{in}}}{2\theta} \right) \exp \left(A - \frac{B}{T} \right) \quad (7c)$$

$$\phi = \frac{c_{A, \text{in}}}{c_{B, \text{in}}} \quad (7d)$$

$$\theta = \frac{(-\Delta H_r) c_{B, \text{in}}}{2 \rho c_p} \quad (7e)$$

The way we in reality obtain the disturbance state from the measurement of the temperature, y :

$$x_d = y - T$$

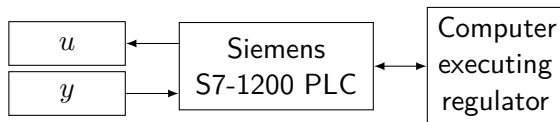
Time delay in the input

$$q(t) = u(t - T_d)$$

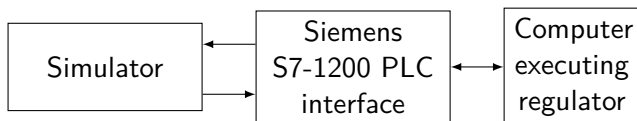
$$T_s = 0.5 \text{ s}, T_d = 1.2 \text{ s}$$

NMPC simulator

It's important to connect to the process



Yet, even more important to connect to a simulator beforehand



Switching between process and simulator is a matter of changing an IP address.

Almost ready for NMPC!

Prerequisites are coming together

- ▶ Model is established, assumptions are acceptable
- ▶ Model augmented with a time-delay to improve fit
- ▶ Satisfactory fit between model and data obtained

NMPC problem

- ▶ Problem solved via. direct multiple shooting
- ▶ Objective function comprises quadratic term and rate of movement input regularization
- ▶ Minimized s.t. constraints: ODE model, input and rate of input change

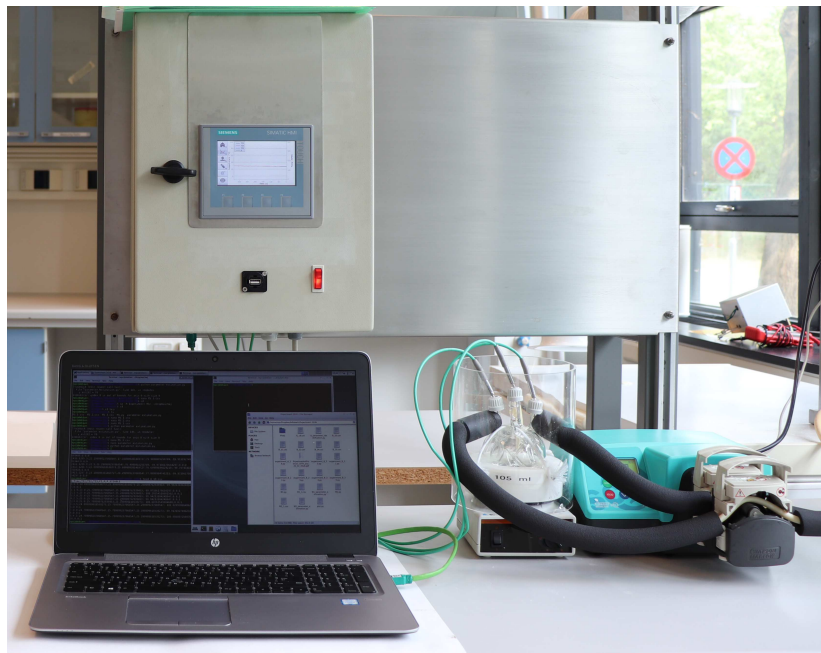
Algorithm



The problem is solved with CasADi in Python.

See `direct_multiple_shooting.py` on their Github for sample code.

Experimental setup



Experimental Procedure

Experiments are performed according to a detailed procedure promoting repeatability and data integrity.

Adiabatic CSTR Experiment Protocol (Release version 1.0)
Manual Page 2
Date/Signature: 1.0/1.0/1.1/1.1

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Adiabatic CSTR Experiment Protocol (Release version 1.0)
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Date/Signature: 1.0/1.0/1.1/1.1

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Preparation of 25 L 1.6 M Na2S2O3

What	Value	Actual Value	Date/Signature
Accurate			1.0/1.0/1.1/1.1
Na2S2O3 (100 g)			
NaClO4 (25 L H2O)			
Assign batch ID		4	1.0/1.0/1.1/1.1
Tare	0 g	0.0 g	1.0/1.0/1.1/1.1
Add	Total mass	99.270 g	1.0/1.0/1.1/1.1
Na2S2O3 (100 g)			
	GAS No.	76702-13-2	
Add hot water	Total mass	21.97 g	1.0/1.0/1.1/1.1
	Total mass	121.24 g	1.0/1.0/1.1/1.1
Add NaClO4 (12.5 g)			
	Total mass	133.74 g	1.0/1.0/1.1/1.1
	GAS No.	499-13-8	
Calculate mass of acetic acid	21.967 g		1.0/1.0/1.1/1.1
Calculate molarity of solution	1.60 M		1.0/1.0/1.1/1.1
Place in freezer	Date	1.0/1.0/1.1/1.1	1.0/1.0/1.1/1.1
	Time	07:44	
In use	Date	1.0/1.0/1.1/1.1	1.0/1.0/1.1/1.1
	Time	10:30	

Titrals according to Determination of Concentration of 1.6 M Na2S2O3

Titration result	Sample ID	V	M	Date/Signature
Titration result I	16	1.8	1.6 M	1.0/1.0/1.1/1.1
	18	1.8 M		
Titration result II	19	3.0	1.6 M	1.0/1.0/1.1/1.1
	1.8 M			
Titration result III	19	3.1	1.6 M	1.0/1.0/1.1/1.1
	1.8 M			

Final solution concentration: 1.6 M Na2S2O3, 1.0/1.0/1.1/1.1

Adiabatic CSTR Experiment Protocol (Release version 1.0)
Manual Page 31
Date/Signature: 1.0/1.0/1.1/1.1

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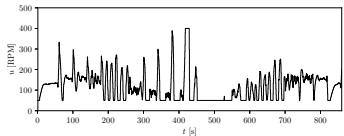
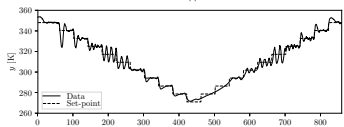
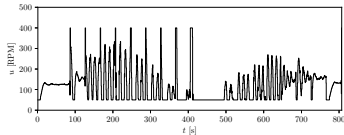
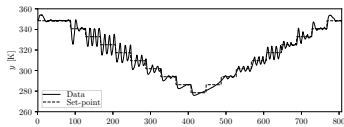
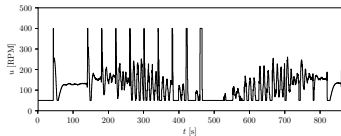
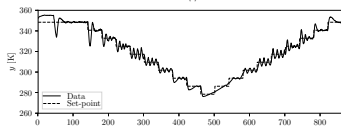
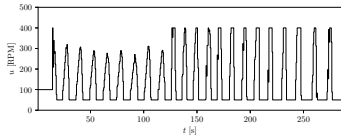
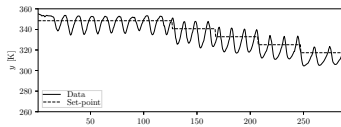
A Identification Experiment

What	Value	Actual Value	Date/Signature
Experiment Identification	Experiment ID	18	1.0/1.0/1.1/1.1
Assign Experiment A ID	Experiment A ID	19	1.0/1.0/1.1/1.1
Identify script used for initialization and data acquisition when a calibration is carried	Experiment A ID	19	1.0/1.0/1.1/1.1
Experiment start	Date	1.0/1.0/1.1/1.1	1.0/1.0/1.1/1.1
After this point is time the script may not be modified	Minutes	10:34	
Experiment end	Date	1.0/1.0/1.1/1.1	1.0/1.0/1.1/1.1
	Minutes	10:50	
Save acquired data as a CSV file where it identifies the current Experiment A ID	File name	1.11.csv	1.0/1.0/1.1/1.1

0.1 M Na2S2O3 Titrals measured: 1.0/1.0/1.1/1.1

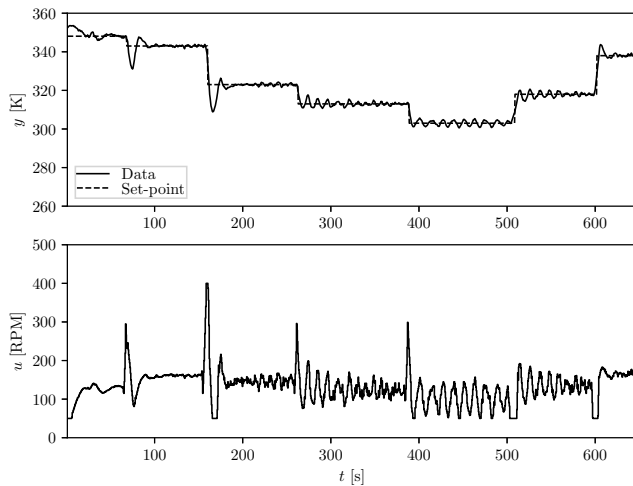
NMPC Results 1-4

Trial 1 to 4



NMPC Results 5

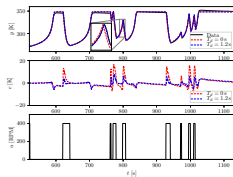
Trial 5 - $T_d = 1.2$, $\alpha = 0.1$, $|\Delta u| \leq 30$



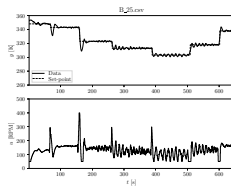
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A non-linear model with input time delay.



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